

CORNSTALK AS A SOURCE OF FIBER AND ENERGY

Aziz Ahmed¹ and J. Y. Zhu²

¹Ecorntech R&D Inc
5406 Upland trail
Middleton, WI 53562
aahmed@fs.fed.us

²USDA Forest Service
Forest Products Laboratory
One Gifford Pinchot Drive
Madison, WI 53562

ABSTRACT

Wood is the major source of fiber supply. Non-wood fibers are mainly used in papermaking where there is a lack of forest resource such as in China and India. Cornstalk, among the agricultural residues and other non-wood fiber, is the most promising source of fiber. However, The usage of cornstalks is very limited in pulp and paper industry, although nearly 284 million tons/year are available worldwide, including 150 million tons/year in the United States. Cornstalk contains about 27% hemicelluloses, which is higher than most of the hardwoods and non-wood fiber materials. Preservation of hemicelluloses in papermaking fiber is important for increased fiber-to-fiber bonding and pulp yield. Unfortunately, in conventional pulping process, most of the hemicelluloses are degraded and ends up in pulping liquor. The calorific value of hemicelluloses derivatives in black liquor is very low compare to lignin derivatives. A value added alternative is to partially extract hemicellulose in cornstalk prior to pulping by dilute acid hydrolysis in the form of sugar suitable for fermentation into ethanol without reducing fiber quality. Dilute acid hydrolysis process under various conditions has been applied for partial removal of hemicelluloses. The residual materials were pulped using soda-AQ process. The separation of hemicelluloses is optimized to protect the paper strength properties.

INTRODUCTION

Recent price hike of petroleum in the world market has given economic incentive to convert renewable lignocellulosic materials into energy. Two stages of acid hydrolysis were suggested to convert the hydrolyte fraction of hardwood into fermentable sugar for the production of ethanol (1,2). Indeed,

several Companies and research institution are in the process of producing ethanol from fermentation of sugar derived from biomass through acid hydrolysis and/or enzymatic hydrolysis (3). In this process, biomass needs to be grounded into small particles to enhance the acidic or enzymatic hydrolysis, which is very energy intensive especially for woody biomass.

In traditional chemical pulping process, most of the lignin, hemicelluloses and part of celluloses are degraded and ended up in black liquor that produces energy through combustion. However, the contribution of hemicelluloses and celluloses derivatives in black liquor in energy conversion is very low compared to those of lignin derivatives. Attempts were taken previously to separate hemicelluloses from wood chips by hydrolysis before proceeding for pulping. In those cases, objectives were to produce rayon grade viscose pulp. Prehydrolysis products were not further processed (4,5). Recent concept of value prior to processing biorefining (6, 7), in which hydrolyzed materials are used for ethanol production through fermentation and solid residues for pulp production, has drawn much attention of scientific community.

Agricultural residues such as cornstalk offer a promising alternative to hardwood and softwood species in terms of fiber as well as energy under value prior to processing concept. Cornstalk contains more hemicelluloses than wood that can be partially extracted prior to pulping without reducing pulp and paper quality. The hemicelluloses in the form of fermentable sugar were extracted to produce ethanol. The average fiber length of cornstalk pulp is similar or better than hardwood pulp. The characteristics of fiber and pulping processes for softwood and hardwood compare to cornstalk are shown in Table 1. In fact, cornstalk pulp can serve as an important raw material for printing, writing and specialty grades paper (8). Many developing countries, where the forest resources are limited, have turned to non-wood plants and agro-based materials for papermaking (9). Currently, the use of agricultural residues for pulp and papermaking in the United States is negligible, although nearly 284 million tons including 150 million tons of cornstalk are annually available (10). The objective of this study is to demonstrate this value prior to processing concept using cornstalk for simultaneous production of fermentable sugar and pulp in laboratory. The study is focused on sugar and pulp yields and pulp quality under various hydrolysis and pulping conditions.

Table 1: Fiber characteristics and pulping processes for wood and cornstalk materials (9-13).

Fiber source	Average fiber length (mm)	Fiber size diameter (micron)	Cellulose (%)	Lignin (%)	Pentosans (%)	Pulping process
Softwood	2.7-4.6	32-43	40-52	26-32	8-12	All
Hardwood	0.7-1.6	20-40	38-50	18-28	15-25	All
Cornstalk	1.0-1.5	18-22	46-50	16-17	27-28	Soda, Kraft

EXPERIMENTAL

Materials

Cornstalk was procured from a farm near Madison in Wisconsin, USA. The cornstalk used in this project was standing in the field throughout the winter and harvested in April. Insect or mold did not deteriorate the cornstalk quality. The humidity level of cornstalk was less than 20% during harvesting. Cornstalk stems were separated manually from the leaves and other unwanted materials. Based on our previous observation, the bottom 3 to 4 ft of cornstalk is the best source of quality fiber (8). Separating the pith from this part is not necessary, since the pith content is relatively low and substantial amount of good quality fibers are present. Cornstalk stems were cut into pieces varying from 2 to 4 cm long and dried in air to a humidity level of 8%.

Hydrolysis and pulping

Dilute sulfuric acid of concentration 0.25, 0.5 and 1% based on oven dry cornstalk was used in prehydrolysis while maintaining the liquor to cornstalk ratio 4:1. The hydrolysis temperature was

Varied from 120⁰C to 140⁰C for a period varied from 15 min to 60 min and a ramp time of 30 min. Cornstalk residues after dilute acid hydrolysis were pulped at 150⁰C for a period varying from 15 to 30 min using liquor with 12% active alkalinity and 0.5% AQ except sample CSP-6 where AQ was not included in the liquor. Cornstalk without prehydrolysis was pulped at 160⁰C for 60 min using liquor containing 12% active alkalinity and 0.5% AQ as control for comparison purposes (sample CSP-4). Sugar analysis of cornstalk and liquid fraction of hydrolysis was carried out by the Analytical Chemistry and Microscopy Laboratory of USDA Forest Products Laboratory (Madison, WI, USA). Handsheets preparation and paper testing were done following the TAPPI methods.

RESULTS AND DISCUSSION

Data in Table 2 lists the results of sugar analysis of the cornstalk sample used in this study. The total carbohydrate in the form of sugar obtained from the sample was 55.6%. The remaining fractions are lignin, extractives and unaccounted.

Table 2 Sugar analysis of cornstalk

Arabinan %	Galactan %	Rhamnan %	Glucan %	Xylan %	Mannan %	Total Carbohy %	Total carbohydrate Yield, %
1.25	0.57	0.04	38.47	15.13	0.11	55.6	55.6

Twenty-seven prehydrolysis experiments were carried out based on a 3 by 3-factorial design in a wide range of acid concentration, reaction temperature and duration. Some data are presented in Table 3 as an example. The yield of solid residues yield from prehydrolysis process ranges from 80 to

90%, thus excessive removal of celluloses/hemicelluloses was avoided. The objective of the prehydrolysis is to remove the cellulosic/hemicellulosic fraction of cornstalk that is easily degraded to soluble products in pulping process.

Table 3 Acid hydrolysis conditions and hydrolysis products

Exp no	Acid conc. %	Temp. °C	Time min	Solid residue, % of cornstalk	Total carbohydrate % of cornstalk	Free Sugar % of cornstalk	Oligomers % of cornstalk	Total carbohydrate % of total carbohydrate in cornstalk
CS-2	0.5	120	15	90	6.86	6.14	0.72	12.34
CS-7	0.25	130	60	86	6.88	5.7	1.18	12.37
CS-12	1.0	120	30	86	4.14	2.98	1.16	7.45
CS-17	0.5	140	15	86	7.39	6.52	0.87	13.29
CS-23	0.5	130	15	88	7.37	6.08	1.29	13.26

Liquid fraction of prehydrolysis products was analyzed for free sugar and the results are listed in Table 3.. However, the prehydrolytic products contain both free sugars and oligomers. Table 4 lists the yields of various components of the five prehydrolysis experiments. Further acid hydrolysis of liquid fraction was done to convert all oligomers into free sugar and the results are listed in Table 5. The results (Table 4 and 5) from the two subsequent

hydrolysis processes were used to calculate the prehydrolysis yields of total carbohydrate, free sugar, and oligomers (Table 3). The total carbohydrate yields based on feed cornstalk varies from 4 to 10% for the 27 experiments conducted but only the results from 5 are listed, which is equivalent to 7 to 19% based on total carbohydrate in cornstalk.

Table 4 Sugar analysis of liquid fraction of hydrolysis process.

Non-hydrolyzed: mg/g(OD) cornstalk as free sugar

Sample	Suc	Arab	Gal	Rham	Glc	xyl	Man	Fruc	Total Carbohyd
CS-2	7.288	0.549	0.100	-	23.862	0.250	-	29.228	61.277
CS-7	2.460	1.240	0.160	-	24.400	0.280	0.520	27.900	56.960
CS-12	0.560	2.140	0.120	0.040	1.200	0.360	-	25.240	29.660
CS-17	0.756	1.617	0.168	-	30.135	0.294	0.252	35.259	68.481
CS-23	0.560	2.380	0.280	-	26.120	0.520	-	30.880	60.740

Table 5 Sugar analysis of hydrolyzed liquid fraction of hydrolysis process. Hydrolyzed: mg/g (OD) cornstalk as free sugar

Sample	Arab	Gal	Rham	Glc	xyl	Man	Total Carbohyd
CS-2	1.171	0.724	-	28.554	1.473	-	31.922
CS-7	2.698	1.400	-	30.140	3.040	1.060	38.338
CS-12	3.284	1.400	-	6.560	3.640	0.700	15.584
CS-17	2.709	1.239	-	33.369	3.318	0.861	41.496
CS-23	3.871	1.640	-	30.620	5.040	0.940	42.111

For comparison purposes, cornstalk without prior hydrolysis was pulped using soda-AQ process and paper properties are presented in table 6. The washed solid residue after acid prehydrolysis was subject to pulping. The solid residues from hydrolysis experiment CS-23 was chosen based on sugar extraction and solid residual amount for pulping. The solid residues were pulped under various cooking conditions. The Canadian standard freeness of the pulp samples from different pulping conditions varied from 500 ml to 600 ml. The pulps were not refined further before handsheet making. The pulp yield (screened) based on initial cornstalk (OD) is around 41.5% except sample CSP-6 where AQ was not used in pulping. Yield is only 38.7% without AQ. AQ gives some protection against cellulose/hemicellulose degradation in pulping process. A 3% pulp yield gain (the difference CSP-6 and CSP-8) was a result of the presence of AQ in the pulping

liquor in CSP-8. The screen reject was around 1.5% in cornstalk pulp, while reject was less than 1% for hydrolyzed solid residues pulp. The pulping of hydrolyzed solid residue required far less drastic condition (pulping temperature and duration) or low H-factor to yield comparable and/or better pulp than that directly derived from cornstalk. Although the pulp yield of direct cornstalk is 44% slightly higher than the yield of hydrolyzed solid residues of 41.5%, the kappa number is 32.8 much higher than 6 to 7 for the later. One would expect the pulp yield for direct cornstalk pulping to drop significantly, below the yield of prehydrolyzed solid residuals, to reach a final pulp kappa number of around 6-7. The brightness of the pulps derived from prehydrolysis run is almost 70% higher than the pulp from direct pulping of cornstalk under the same alkalinity.

Table 6 Pulping conditions of hydrolyzed and non-hydrolyzed (CSP-4) cornstalk and paper properties

Sample	Cook time, min	Screened yield, % of initial cornstalk	Kappa No	CSF, ml	ISO-brightness %	Scatt. Coeff. m ² /kg-	Tensile index, N-m/g	TEA J/m ²	Burst index, kPa-m ² /g	Tearing index mN-m ² /g
CSP-4	60	44	32.8	600	23.5	23.1	98	97	4.9	6.1

CSP-6	30	38.7	9.2	600	39.5	21.3	97	90	5.0	6.1
CSP-7	15	41.6	6.5	550	39.4	20.5	106	108	5.72	6.4
CSP-8	30	41.7	5.9	552	39.1	21.2	104	103	5.8	6.0

Light scattering coefficient is a measure of the degree of bonding in paper and generally inversely proportional to paper strength properties. The scattering coefficient of the handsheet from direct pulping cornstalk is higher than those from hydrolyzed cornstalk solid residues, suggesting poor bonding. The prehydrolysis runs (except the CSP-6 that was cooked without AQ) also produced paper with equivalent tear strength and higher tensile energy absorption (TEA), tensile index, and burst index than the direct pulping run. The results in Table 5 also demonstrate the importance of having hemicelluloses in the pulp. Sample CSP-6, where hemicellulose protector was not used, showed lower tensile and burst strength than CSP-8, in which AQ was used. The paper properties in Table 5 clearly demonstrate the feasibility of prior separation of certain fraction of carbohydrates in the form of fermentable sugar without affecting the paper making quality of cornstalk.

CONCLUSION

Cornstalk that contains high hemicelluloses and low lignin compare to wood is a potential source of energy and papermaking fiber. It is possible to extract 10 to 15% of the total carbohydrate in cornstalk through dilute acid hydrolysis prior to pulping without affect paper properties. Moreover, pulping process will require a lower cooking temperature and short cooking time (or lower H-factor) than direct pulping of cornstalk. Pulp produced from hydrolyzed cornstalk shows higher brightness, lower kappa number, and higher paper strength properties than the pulp from direct pulping of cornstalk.

REFERENCE

1. Springer, L.E., Prehydrolysis of hardwoods with dilute acid., Ind. Eng. Chem. Prod Res. Dev., 1985, 24, 614-623
2. Harris, J.F., Baker, A. L., et al, Two Stage dilute acid hydrolysis of wood: An investigation of fundamentals: USDA Forest Service: Madison WI 1985
3. Iogen Corporation, Demonstration plant to prove the feasibility of Iogen's cellulose ethanol process. <http://www.iogen.can/>
4. Rydholm, S. A., Pulping Processes, Interscience, New York, 1965, Chapter 9, p 649.
5. Arhlpainen, B., Nevalainen, P. et al., Development of the Alva prehydrolysis process, In: Proceedings of the TAPPI Pulping Conference, Technical Association of the Pulp and Paper Industry, Atlanta, 1981, pp 399-416.
6. Kelley, S.S., Forest Biorefineries: Reality, hype or something in between?, Paper Age, 2006 (March/April), 46-48
7. Raymond, D., and Closset, G., Forest Products biorefinery: Technology for a new future, 2004, (September), 49-53.
8. Won, J.M. and Ahmed, A., Cornstalk as a raw material for papermaking, In: Proceedings of the 58th Appita Annual Conferences and Exhibition, Melbourne, Australia, 2004, vol. 1, p 5-11, Publisher: Appita
9. Atchison, J., Update on global use of non-wood plant fibers and some prospects for their greater use in the United States, In: Proceedings of the North American Non-wood Fiber Symposium, Atlanta, Georgia, 1998, Tappi Press, 1998.
10. Rowel, R., Young, R. and Rowel, J., Editors, Paper and Composite from Agro-based Resources. Publisher: Lewis publisher, New York, London, 1997.
11. Fengel, D. and Wegener, G. Book: Wood Chemistry, Ultrastructure, Reaction, Publisher: Walter de Gruyter, Berlin, New York, 1984
12. Watson, A.J. and Gartside, G., Utilizing non-woody fiber from agricultural crops, Australian Forestry, 39(1): 16-22(1987).
13. Kocurek, M.J., Hamilton, F. and Leopold, Eds. Pulp and Paper Manufacture, vol.3, secondary fibers and non-wood pulping, Tappi press, Atlanta, Georgia, 1987.

Aziz, Ahmed; Zhu, J.Y. 2006. Cornstalk as a source of fiber and energy. In: Proceedings of 3rd international symposium on emerging technology of pulping and papermaking; 2006 November 8-10; Guangzhou, China; Guangzhou, China: South China university of technology press: (new technologies in non-wood fiber pulping and papermaking; Huaiyu, Zhan; Fangeng, Chen; Shiyu, Fu, eds.;;) 1-4.